

The Town of Leesburg



Water Pollution Control Facility









The Town of Leesburg, Virginia Water Pollution Control Division Mission Statement

The Water Pollution Control Division (WPCD) is responsible for the safe and efficient treatment of all wastewater generated within the Leesburg Service Area, and the subsequent stabilization and disposal of the solid wastes produced, to ensure the protection of public health and the environment. This responsibility includes the operation of the Water Pollution Control Facility, Dechlorination/Outfall Facility, remote wastewater pumping stations, management of the sludge application sites, and the two WPCD laboratories (a total of 36 buildings plus 73 treatment-unit structures). These responsibilities also include monitoring of WPCD personnel training requirements and compliance with numerous federal, state, and local regulations. Additional responsibilities include calibration and maintenance of all town portable gas meters; and response to environmental complaints or requests for assistance from town citizens and consultants.







elcome to the Town of Leesburg's Water Pollution
Control Facility. The processes and equipment used
to treat the town's wastewater are some of the most
sophisticated state-of-the-art technology in the industry. The facility's
design, construction, and operation meet the requirements of many
regulatory agencies. To ensure compliance with all federal, state, and local
regulations, permits for discharging treated effluent into the Potomac River,
biosolids reuse, and air emissions from the operations of an emergency
generator, a sludge dryer, a fired boiler, and a digester gas flare have been
issued by the Virginia Department of Environmental Quality (DEQ).
The result of maintaining regulatory compliance is a safe and clean
environment for many future generations.



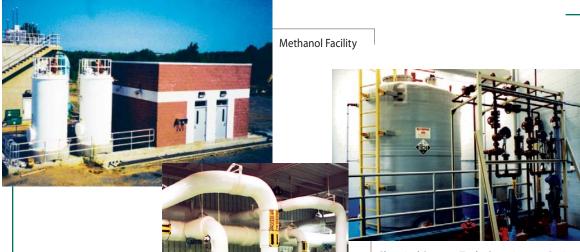
Reactor Basins (right) Reactor Basin Being Serviced (above)

The Town of Leesburg has worked to reduce water pollution since the construction of its original wastewater treatment plant in 1939. That facility was located on Catoctin Circle and expanded once in 1955. The current facility was constructed in 1970 as a result of growth within the town. It was capable of treating 1.3 million gallons per day (mgd) of wastewater. The site along Market Street, State Route 7, adjacent to Tuscarora Creek was chosen as an ideal plant location. It was further downstream on Tuscarora Creek, which received the treated effluent, and would allow areas for town growth as well as for treatment plant expansion.

Over the years, the facility has undergone many upgrades and expansions. In 1974, a chemical-feed building was built. Ferric chloride and polymer were introduced into the treatment process for improvements in biochemical oxygen demand and removal of total suspended solids. In 1976, agricultural land application of stabilized sludge began. This method has proved to be a cost-effective and environmentally safe means of solids disposal. Because of growth and improvements made to the plant, a maintenance shop was constructed in 1980 to house the spare parts and equipment necessary for maintaining all of the complex equipment.

As the town continued to grow through the 1970s and early 1980s, the raw-wastewater collection system expanded proportionally. The Cattail Branch drainage basin, including a new Cattail Branch Pump Station; and the Sycolin Creek drainage basin, including the associated Airport Pump Station; were added to the town's sewagecollection system. A major plant upgrade and expansion was developed and approved by the town government to meet these increasing needs, provide capacity for continued growth into the 1990s, and improve system reliability and take advantage of improvements in process technology. In 1988, the





Centrifugal Blower For Process Air

Chemical Storage Tank, Containment Basin, And Chemical Pump Feed System

Water Pollution Control Facility was expanded to a capacity of 2.5mgd average flow under a 90-percent funded EPA grant. In addition to increased treatment capacity, the plant was outfitted with variable-speed influent pumps, gravity sand filters for a tertiary level of treatment, and a belt filter press for sludge processing when land application of liquid sludge is not feasible. Emergency storage basins and a diesel-powered emergency generator also were added to improve system reliability.

In an effort to make the plant as efficient as possible, more improvements were made from the 1980s into the 1990s. In 1989, the recently abandoned chlorine-contact tank was converted into a receiving station. Wastewater from sewerline cleaning operations could

quickly and easily be discharged and introduced into the plant influent by simply unloading at this structure. In addition, because of the plant's continuing expansion and an imminent second upgrade and expansion, a maintenance storage building was constructed in 1994 to house spare parts and equipment, allowing more room in the existing shop for performing maintenance and repairs.

As expected, the town continued to grow. The Big Springs drainage basin, including the Big Springs Pump Station, was added to the collection system. For reasons similar to those for the first upgrade and expansion, the town again decided to enlarge and improve the Water Pollution Control Facility. In 1995, new structures and systems that allow

for treating 4.85-mgd average flow were initiated. This upgrade included using many new technologies for improving the level of treatment, incorporating new management philosophies for economic and efficient plant operation, and increasing the personnel's safety. The improvements included adding nitrification capabilities and phosphorous-removal capabilities, replacing gaseous chemicals with liquid forms, constructing containment basins for all chemical-storage tanks, raising the elevations of structures in the 100-year floodplain to prevent flooding of these facilities, creating a central onsite stormwater-collection system and containment basin, providing a water-reuse system for onsite needs to save 350,000 gallons per day of potable water (thereby



Plant Water Pump Station

increasing the capacity of the potable water treatment plant and the Water Pollution Control Facility), using oxidationreduction potential to control disinfection, incorporating sophisticated process instrumentation and controls with monitoring capabilities through a plant-wide distributed control system, adding a 340,000-gallon sludge-storage tank, constructing a dewatered-sludge storage pad for dried-sludge storage, and many other improvements. One significant change to the wastewater treatment process was relocation of the planteffluent discharge. A new pump station, pipeline, and outfall structure were constructed to allow effluent to discharge into the Potomac River downstream of the town's water treatment

plant. This change moves the treated effluent discharge from Tuscarora Creek, which is part of the Dulles Area Watershed, directly to the Potomac River and thereby decreases in-water concentration from 100 percent to 0.8 percent.

The tremendous growth in Loudoun County through the 90's and at the turn of the century required town utility services to keep pace. New pump stations at Potomac Crossing, Old Waterford Knoll, Cattail Branch, and Goose Creek were constructed to accommodate new growth and development in those areas. Reuse of plant effluent is a sustainable and economical solution for improving the environment and gaining in popularity across the country. The town has taken advantage

of this concept by supplying effluent water for irrigation of a local golf course. To assist in the cleanup and protection of the Potomac River and Chesapeake Bay, the town voluntarily entered an agreement with the Commonwealth of Virginia for a 50/50 cost sharing program to study, design and construct a plant upgrade that cost-effectively converted the treatment process to one with biological nitrogen removal (BNR) capabilities. This new process, completed in mid-2001, significantly reduces the concentration of nitrogen discharged into the environment, thus reducing the growth of algae and other undesirable aquatic vegetation. This upgrade, which added several new structures to the 30-year-old plant, is just another example of





Soil Amendment Storage Building

the town's commitment to a safe and clean environment.

Treated effluent is discharged into the Potomac River, under a discharge permit issued by the Virginia DEQ. The current discharge limits mandated by DEQ are as follows:

Flow 7.5 (mgd)

5-day Biological

Oxygen Demand 10 (mg/L)

Total Suspended Solids 10 (mg/L)

Total Kieldahl/Nitrogen 3.0 (mg/L)

as Nitrogen (5/1 - 10/31 only)

Total Phosphorus 2.0 (mg/L)

Total Nitrogen 8.0 (mg/L)

E. Coli 200 (N/Cml)
TR Chlorine Nondetectable

Nondetectable (mg/L)

Dissolved Oxygen 5.0 (mg/L)

pH 6.5 - 8.5 (SU)

The discharge limits are met by treating the wastewater in a series of traditional and sophisticated treatment processes, briefly described below.

Preliminary Treatment: removes large objects and heavy inorganic matter (grit) from the wastewater.

Primary Treatment: uses physical and chemical processes to remove the majority of settleable and floatable organic matter.

Secondary Treatment: uses biological and physical treatment processes to reduce the amount of ammonia and of suspended and dissolved organic matter in the wastewater.

Advanced Secondary Treatment: uses a physical process to remove suspended solids from the wastewater.

Tertiary Treatment: uses a chemical process to remove phosphorous and biological and physical processes to remove nitrogen from the wastewater.

Final Treatment: a series of three processes—disinfection, dechlorination, and effluent aeration—that completes the treatment before the wastewater is discharged into the Potomac River.

Odor Control Biofilter





Solids Processing Building and Odor Control RTO

Odor Control Covers at Gravity Thickener

An organic by-product is generated during the wastewater treatment process. This biosolid material has been traditionally thickened and stabilized to meet regulated Class-B biosolids treatment standards. The treated biosolids were then applied in liquid form to local farmlands. At the end of 2001, the town completed a state-of-the-art facility, the first in Virginia, to heat-dry the solids and produce a Class-A, pathogenfree, granular product. The project that built the dryer system included facilities and equipment capable of thickening, dewatering, transporting, and storing the product. This biosolids product, can be hauled off in bulk form, in open commercial trucks, or sealed in 25- or 50-pound bags for convenient distribution and use by individuals. Because the pellets are organic, they are ideal for use on gardens, farms, lawns, etc. Leesburg's safe and creative reuse of biosolids is yet another example of the town's commitment to the environment and a business approach

The waste solids are processed in several steps, which are described briefly in the following summaries:

Thickening: increases the concentration of solids to improve

anaerobic digestion, increase storage capacity, and

reduce operating costs.

Digestion: uses a biological treatment process to thicken

and stabilize the sludge in a heated anaerobic environment so that it is safe for disposal.

Storage: provides further thickening while the solids awaits

dewatering or disposal.

Blending: combines solids generated from various sources (i.e.

digested and activated solids) to optimize handling

and increase thickening.

Dewatering: removes water from digested solids to prepare it for

drying or storage on the solids-storage pad when the heat dryer equipment is not operating or land

application of liquid sludge is not feasible.

Heat Drying: dries the blended, dewatered solids at temperatures

in excess of 1,200 degrees F to destroy all pathogenic organisms and improve material

handling and storage.

After the biosolids have been stabilized, they are ready for reuse. The Virginia Department of Agriculture and Consumer Services (VDACs) and DEQ have approved a program allowing the use of this material through farmland application, distribution, or marketing.



to government.

In 2008, the Water Pollution Control Facility was expanded to a capacity of 7.5 mgd average flow. Many facilities have been constructed with future capabilities to facilitate an expansion to 10 mgd average flow, including a new influent pump station with a new influent receiving box, hydraulic operated fine bar screens with wash presses, and a new effluent pump station, each capable of handling the peak flows for a 10 mgd plant. In addition, two new BNR reactor basins, two new secondary clarifiers, a new

diurnal flow splitter structure and one emergency storage tank were constructed. Modifications to Solids Processing included installation of a new gravity belt thickener, and replacement of existing belt filter press feed pumps and grinders.

The Water Pollution Control Facility now has a plant-wide approach to controlling odors from liquids and solids processes. An odor control system consisting of two built-in-place biofilters and one regenerative thermal oxidizer (RTO) were installed during the Upgrade and Expansion Project 7.5.

Combined, the biofilters and the RTO, treat approximately 40,000 cfm of odorous air from 7 different sources.

To minimize air emissions from the plant, a new and more efficient generator was installed to replace the two older less efficient generators. This generator also provides backup power generation for the plant's increased treatment capacity.

As the Town of Leesburg expands, it will continue being a responsible steward of public health and the environment.

1939 ORIGINAL WATER POLLUTION CONTROL FACILITY

Design Engineer: The Rust Engineering Company
Construction Contractor: W.C. Spratt Contractors

1970 WATER POLLUTION CONTROL FACILITY AND TUSCARORA INTERCEPTOR

Design Engineer: Johnson & Williams Treatment Capacity: 1.3 mgd
Construction Manager: Johnson & Williams Project Cost: \$1.3 million

Construction Contractor: English Construction

1988 UPGRADE AND EXPANSION

Design Engineer: Betz-Converse-Murdoch Treatment Capacity: 2.5 mgd
Construction Manager: Camp, Dresser & McKee Project Cost: \$9.7 million

Construction Contractor: R. F. Kline

1995 EXPANSION AND EFFLUENT PIPELINE

Design Engineer: CH2M HILL Treatment Capacity: 4.85 mgd
Construction Manager: CH2M HILL Project Cost: \$17.2 million

Construction Contractor: M. A. Bongiovanni

2001 BNR AND BIOSOLIDS UPGRADE

Design Engineer: CH2M HILL Treatment Capacity: 4.85 mgd
Construction Manager: CH2M HILL Project Cost: \$17.5 million

Construction Contractor: Bearing Construction

UPGRADE AND EXPANSION 7.5

Design Engineer: CH2M HILL Treatment Capacity: 7.5 mgd
Construction Manager: CH2M HILL Project Cost: \$37.5 million

Construction Contractor: Ulliman Schutte Construction

LIQUID TREATMENT

FLOWS

7.50 MGD = 5208 Gal/MIN Average Day: Maximum Month: 9.00 MGD = 6250 Gal/MIN Peak Hydraulic Capacity: 18.75 MGD = 13021 Gal/MIN

PRELIMINARY TREATMENT

Mechanical Screens: 2 Units 45 MGD Each Capacity: Opening Size: 3/8 Inch

Raw Sewage Pumps: Submersible:

6 Variable Speed 4 @ 6,000 GPM Each Capacity: 2 @ 3,000 GPM Each 84-168 HP Each Horsepower: **Emergency Storage Basins:** 2 Units

1.25 MG Each Capacity: Emergency Storage Tank: 1 Unit

PRIMARY TREATMENT

Capacity:

Primary Clarifiers: 3 Units

60 Ft Diameter 211,385 Gals Each 10 Ft SW Depth 634,150 Gals Total

1.8 MG

Primary Scum System: 2 Units

SECONDARY TREATMENT

Recycle Equalization Basin 1 Unit 169,100 Gals Each 60 Ft Diameter 8 Ft SW Depth 507,300 Gals Total Retention Basins A/B: 2 Units

473,900 Gals Each 24 Ft x 120 Ft 22 Ft SW Depth 947,800 Gals Total Membrane Diffusers 482 Per Basin Mixers 3 Per Basin **Internal Recycle Pumps** 2 Per Basin

Retention Basins C/D: 2 Units 70 Ft x 165 Ft 814,500 Gals Each 22 Ft SW Depth 1,629,000 Gals Total Membrane Diffusers 914 Per Basin

Mixers 3 Per Basin 2 Per Basin Internal Recycle Pumps Retention Basins E/F: 2 Units 6,250,000 Gals Each 24 Ft x 165 Ft

22 Ft x SW Depth 1,250,000 Gals Total Membrane Diffusers: 731 Per Basin 3 Per Basin Mixers Internal Recycle Pumps 2 Per Basin **Secondary Clarifiers:** 4 Units 40 Ft x 160 Ft 765,950 Gals Each

TERTIARY TREATMENT

16 Ft SW Depth

Nitrification: Performed in Activated Sludge System

3,000,000 Gals Total

Performed with FeCl3 in Phosphorous Removal: **Primary Clarifiers**

2 Units

Gravity Sand Filtration:

26,000 Gals Each 11 inches of 0.58 MM sand 54,000 Gals Total 4.85 MGD Capacity

POTOMAC RIVER DISCHARGE SYSTEM

Effluent Pumps: 6 Variable Speed 2600-3500 GPM Each Capacity 250 HP Each Horsepower Non-Potable Pumps: 6 Variable Speed Capacity 325 GPM Each

Effluent Pipeline:

17,000 Feet Pipe 534,000 Gals 7.5 MGD = 95 MIN **Detention Time** 18.75 MGD = 38 MIN

Outfall Structure: 2 Cascades 46 Ft Vertical Drop

SOLIDS TREATMENT

SCREENING

Primary Sludge Screen 1 Unit 500 GPM Capacity

THICKENING

Gravity Thickeners: 2 Units

22 Ft Diameter 30,000 Gals Each 60,000 Gals Total 10 Ft SW Depth WAS Thickening Centrifuge: 1 Unit 100 GPM Capacity

2 Units/2 Reactors WAS Gravity Belt Thickener: 600 GPM

Capacity

STABILIZATION Anaerobic Digesters: 4 Units

30 Ft Diameter 112,400 Gals Each 25 Ft SW Depth 449,600 Gals Total

STORAGE

Sludge Storage Tank: 2 Units 42 Ft Diameter, 33 Ft SWD: 300,000 Gals

DEWATERING

Sludge Holding Tank: 2 Units

1,600 LBS Dry Solids/HR Capacity:

Belt Filter Press: 2 Units 2 Meter: 200 GPM Sludge Storage Pad: 1 Unit 140 Ft x 60 Ft 90 Days Storage

Heat Drying: 1 Unit **Evaporation Capacity** 2,000 kk H₂0/HR Pellet Storage Silos 7 Silos/4,000 FT² Each

DISPOSAL

1,600 Gals Capacity Field Gymmy: Sludge Tanker: 6,000 Gals Capacity 14 Sites on 2 Farms: 285 Acres Total

CHEMICAL SYSTEMS

Ferric Chloride System: 2 Tanks **Primary Clarifier Influent:** 5,000 Gal Each

Secondary Clarifier Influent: Sodium Hydroxide System: 2 Tanks

Aeration Basin Influent 5,000 Gal Each Gravity Filter Influent

Sodium Hypochlorite

System: 2 Tanks Raw Influent 5,000 Gal Each

RAS Wet Well

Secondary Scum Wet Well Gravity Filter Splitter Box

Sodium Bisulfite System: 1 Tank Final Effluent 5,000 Gal **Anionic Polymer System:** 2 Units

Primary Clarifier Influent **Emulsion Feeders**

Secondary Clarifier Influent

Gravity Filter Influent

Cationic Polymer Systems: 3 Units Gravity Thickener Influent Solution Feeder WAS Thickening Centrifuge **Emulsion Feeder** Belt Filter Press Solution Feeder

Methanol System: Reactor Basin Influent 3,000 Gal Each

ODOR CONTROL SYSTEMS

Biofilter:

15,700-18,600 CFM Capacity: EBRT: 45 Seconds

RTO: 1 Unit 10,000 CFM Capacity:





"The Town of Leesburg in Virginia" looking north at intersection of King Street (U.S. Route 15) and the Route 7 and 15 bypass



